

CONTROL VOLUME APPROACH

Yesterday, we discussed that

- Hydrologic cycle (and phenomena) are highly complex
- For simplicity - we adopt systems concept to analyse hydrologic processes.
- One method to use systems concept is control volume approach.
- We have also seen various classification of hydrological models.

Today we will see how we can use the control volume method to analyse hydrological processes.

As discussed we require a three dimensional frame of reference in space with boundaries that enclose to form a volume - called control volume (CV).

Reynolds Transport Theorem

* So in any arbitrary CV the physical laws like



→ conservation of mass, momentum, energy, etc. are valid.

* If you recall fluid mechanics - the Lagrangian and Euler approach to view motion (of objects or particles, etc.).

(2)

- * In Lagrangian ~~analysis~~ approach, the focus is on the motion of a body (when you apply physical laws) and the analysis follows the body wherever it moves.

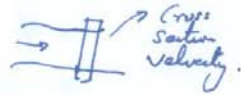


Used in solid mechanics

- * In fluids, we are not interested in individual fluid particle motion.

Fluid is continuous - the motion is analysed in fixed frame in space (CV) through which fluid passes.

This is Eulerian view of motion



- * As studied in fluid mechanics to relate the Lagrangian and Eulerian analysis we need to incorporate substantial or material derivative.

- * RTT gives the equation for material derivative of any extensive fluid property.

- * Therefore, RTT uses the physical laws and applies them on the fluid flowing continuously through the CV.

→ There are two types of fluid properties

- ↳ Extensive
- ↳ Intensive

(3)

→ Extensive properties are those that are related to the mass of fluid present in the CV. You may say B.

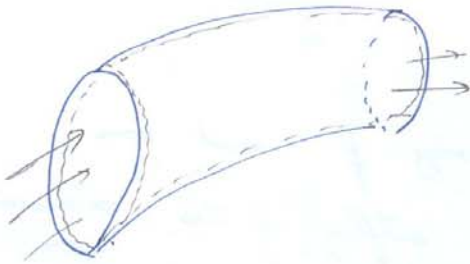
→ Intensive properties are independent of mass.

Symbolically given as β .

β can also be defined as the quantity of that property B per unit mass of fluid.

Some of the extensive properties are
→ Mass, Momentum, etc.

Some intensive properties are
→ Velocity, specific energy, etc.



For any
arbitrary CV
(the dotted black line)

the extensive property

$$B = \iiint \beta \rho dU$$

where dU is elementary volume for integration

Without going into the derivation of RTT,
the equation is given as:

$$\frac{D}{Dt} B = \frac{d}{dt} \iiint_{CV} \beta \rho dU + \iint_{CS} \beta \rho \vec{V} \cdot \hat{n} dA \rightarrow (1)$$

The explanation to this equation is:

(4)

→ The material derivative of or time rate of any extensive property in the CV is equal to sum of the time rate of ^{change of} the extensive property stored inside the control volume and the net outflux of the extensive property through the surfaces of this control volume.

→ If your CV is fixed in space and time (i.e. non deformable) you will get

$$\frac{DB}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \beta S dV + \iint_{CS} \beta S \vec{V} \cdot \hat{n} dA$$

See the physical meaning of second term

→ It is the net outflux of the extensive property.

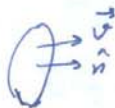


On the left side

$\vec{V} \cdot \hat{n}$ can be negative

On the right side

$\vec{V} \cdot \hat{n}$ can be positive



On the curved surfaces around there

is no flow.

Then, $\vec{V} \cdot \hat{n} = 0$.

(5)

Continuity Equation

Let us take the continuity principle or principle of conservation of mass for a fluid control volume.

Your RTT is :

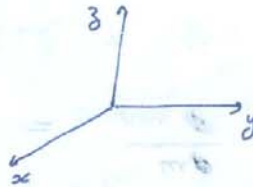
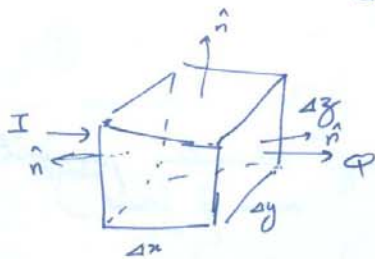
$$\frac{DB}{Dt} = \frac{d}{dt} \iiint_{cv} \rho \, dV + \iint_{cs} \rho \, \vec{V} \cdot \hat{n} \, dA$$

$$\text{Now } \rho = m$$

$$\rho = 1$$

As per conservation of mass principle $\frac{Dm}{Dt} = 0$.

$$\therefore 0 = \frac{d}{dt} \iiint_{cv} \rho \, dV + \iint_{cs} \rho \, \vec{V} \cdot \hat{n} \, dA$$



Let us consider a fixed CV in the space

$$dV = \Delta x \Delta y \Delta z$$

- The rectangular box has volume = $\Delta x \Delta y \Delta z$
- It has six faces.
- Let us assume the flow is present only in y-direction.

(6)

The term $\iint_{CS} \rho \vec{v} \cdot \hat{n} dA = \rho (\vec{v} \cdot A)_{\text{outlet}} - \rho (\vec{v} \cdot A)_{\text{inlet}}$

~~$= \rho \phi - \rho I$~~

$\frac{d}{dt} \iiint_{CV} \rho dV = \rho \frac{dS}{dt}$ where $S = \text{Stress} = CV$.

(Assuming the fluid is incompressible).

$\therefore \rho \frac{dS}{dt} = 0 = \rho \frac{dS}{dt} + \rho \phi - \rho I$

i.e. $\frac{dS}{dt} = I - \phi$

This is the continuity equation that are used for unsteady flow in hydrology.

Momentum Equation

Momentum = $\beta = m \vec{v}$

$\therefore \beta = \frac{m \vec{v}}{dm} = \vec{v}$ (Momentum per unit mass of fluid).

$\therefore$ RTT gives

$\frac{D\beta}{Dt} = \frac{d}{dt} \iiint_{CV} \beta dV + \iint_{CS} \beta \rho \vec{v} \cdot \hat{n} dA$

Now as per Newton's second law the rate of change of momentum is equal to the net force acting on the body.

(7)

$$\therefore \frac{D\vec{B}}{Dt} = \frac{D}{Dt}(m\vec{v}) = \sum \vec{F}$$

$$\therefore \sum \vec{F} = \frac{d}{dt} \iiint_{cv} \vec{v} \rho dV + \iint_{cs} \vec{v} \rho \vec{v} \cdot \hat{n} dA$$

The meaning here is :

$$\begin{array}{l} \text{The net force acting} \\ \text{on the fluid } cv \end{array} = \begin{array}{l} \text{Rate of change} \\ \text{of momentum stored} \\ \text{inside the } cv \end{array} + \begin{array}{l} \text{The Net} \\ \text{Outflow of} \\ \text{Momentum through} \\ \text{the control surface} \end{array}$$

RTT in Energy Balance Equation

We need to balance all inputs and outputs of energy to and from a system (cv).

Say, if E is the amount of energy in a fluid cv, it can be actually sum of internal energy E_u ,

kinetic energy $\frac{1}{2} m v^2$, potential energy mgz

$$\therefore E = E_u + \frac{1}{2} m v^2 + mgz$$

The extensive property $B = E$

$$\therefore B = \frac{E_u}{m} + \frac{v^2}{2} + gz$$

↓
 e_u (internal energy per unit mass)

$$\therefore \frac{DE}{Dt} = \frac{d}{dt} \iiint_{cv} (e_u + \frac{v^2}{2} + gz) \rho dV + \iint_{cs} (e_u + \frac{v^2}{2} + gz) \rho \vec{v} \cdot \hat{n} dA$$

⑧

As per first law of thermodynamics :

$$\begin{aligned} \text{" Net rate of energy transfer into the fluid} \\ = \text{Rate at which heat is transferred into the fluid} \\ - \text{Rate at which fluid does work on its} \\ \text{surrounding} \end{aligned}$$

$$\therefore \frac{DE}{Dt} = \frac{dH}{dt} - \frac{dW}{dt}$$

$$\begin{aligned} \therefore \frac{dH}{dt} - \frac{dW}{dt} &= \frac{d}{dt} \iiint_{cv} \left(\rho u + \frac{\rho v^2}{2} + \rho g z \right) dV \\ &+ \iint_{cs} \left(\rho u + \frac{\rho v^2}{2} + \rho g z \right) \delta \vec{r} \cdot \hat{n} dA \end{aligned}$$