## **STREAM FUNCTIONS (CONTD...)**

Yesterday, we were giving geometric interpretations to stream functions.

- ➢ For incompressible, inviscid, irrotational flow in two-dimensions (i.e., horizontal plane), you saw that the fluid flow can be described in steady state conditions as:  $\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} = 0 \qquad \Rightarrow \boxed{1}$
- So, subsequently you were told that in any xy plane, where the above fluid flow is valid, you can solve equation 1 and get values of  $\psi(x,y)$ .
- > You can do contour plotting and develop streamlines for the flow as shown below:



- > You were also informed that along a streamline, the value of  $\psi$  is constant.
- ➤ If we take any arbitrary control surface through which streamlines go 1
- Consider two points 1 and 2 on an elemental control surface of length 'ds'. The streamlines, (i.e., line in direction of velocity vector) is as shown below:



Let this elemental length on control surface be represented as vector  $(\overrightarrow{ds}) \ge 1$ (Unit direction perpendicular to paper, here).  $\overrightarrow{ds} = dx\hat{\iota} + dy\hat{j}$ 

(Note: We are talking about two-dimensional horizontal flow)

- The unit vector normal to the control surface is given by  $\hat{n} = \frac{dy}{ds}\hat{i} \frac{dx}{ds}\hat{j}$ i.e., the relation  $ds.\,\hat{n} = 0$  $(dx\hat{i} + dy\hat{j}).\left(\frac{dy}{ds}\hat{i} - \frac{dx}{ds}\hat{j}\right) = 0$  (is true).
- > The volumetric flux across this elemental control surface is given as dQ  $dQ = (\vec{v}.\,\hat{n})dA$ where dA = dsx1 $\Rightarrow dQ = (u\hat{i} + v\hat{j})\left(\frac{dy}{ds}\hat{i} - \frac{dx}{ds}\hat{j}\right).ds = \left(\frac{\partial\psi}{\partial u}\hat{i} - \frac{\partial\psi}{\partial x}\hat{j}\right)\left(\frac{dy}{ds}\hat{i} - \frac{dx}{ds}\hat{j}\right)ds$

$$= \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy$$
  
i. e.,  $dQ = d\psi$ 

That is, change in  $\psi$  across the elemental surface is equal to the volumetric flux through the surface.

Therefore, volumetric flux(or discharge) between any two streamlines  $\psi_1$  and  $\psi_2$  is:  $\int_1^2 dQ = \int_1^2 d\psi = \psi_2 - \psi_1$ 



## Example (As adopted from FM White's Fluid Mechanics)

In a flow field, the velocity components were evaluated as  $u=a(x^2-y^2)$ , v=-2axy, w=0

Check whether you can form a stream function for this flow field. If so, what is the stream function?

**Solution:**  $u = a(x^2-y^2)$ v = -2axy

As w=0, the flow is 2-dimensional, we need to check whether the flow is incompressible. (Note: For incompressible fluid  $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$ ).

$$\frac{\partial u}{\partial x} = 2ax, \qquad \frac{\partial v}{\partial y} = -2ax$$
$$So, \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

That is fluid is incompressible and the continuity equation  $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$  is satisfied. Therefore, we can define the scalar stream function  $\psi$  for the given problem.

As 
$$u = \frac{\partial \psi}{\partial y} = a(x^2 - y^2)$$
  
 $\Rightarrow \psi = \int u dy + f(x)$   
 $\Rightarrow \psi = ax^2y - a\frac{y^3}{3} + f(x)$   
 $\Rightarrow \frac{\partial \psi}{\partial x} = 2axy + f'(x)$   
 $\Rightarrow 2$ 

You know  $v = -\frac{\partial \psi}{\partial x} = -2axy$ 

$$\Rightarrow \frac{\partial \psi}{\partial x} = 2axy$$
  
Here in 2,  $f'(x) = 0$   
Or,  $f(x) = \text{constant C}$   
$$\Rightarrow \psi = ax^2y - a\frac{y^3}{3} + C$$

## **Example** (As adopted from FM White's Fluid Mechanics)

Long back in control volume analysis, you had worked out on a sluice gate problem, if you recall. Now list all the boundary conditions needed to solve this flow using differential analysis.

Solution:



In differential analysis, we need to find the values of the dependent variables in each and every point inside the domain. Here the domain can be assumed to be two-dimensional in y-z plane. That is u=0

- $\rightarrow$  As open channel flow is considered, the fluid will be incompressible.
- Moreover, isothermal conditions can be assumed to prevail. Therefore, temperature variations are not included in the analysis here.

The governing equations are:

$$\frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad \text{(Conservation of mass)}$$

$$\rho g_x - \frac{\partial p}{\partial x} + \mu(0) = 0$$

$$\rho g_y - \frac{\partial p}{\partial y} + \mu \left[ \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right] = \rho \left[ \frac{\partial v}{\partial t} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right]$$

$$\rho g_z - \frac{\partial p}{\partial z} + \mu \left[ \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right] = \rho \left[ \frac{\partial w}{\partial t} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right]$$

Also recall,  $\vec{g} = 0\hat{i} + 0\hat{j} - g\hat{k}$ , velocity is uniform at left and right sections (i.e., it is also steady).

Therefore, the equations are:

$$\frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$
$$-\frac{\partial p}{\partial y} + \mu \left[ \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right] = \rho \left[ v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right]$$
$$-\rho g - \frac{\partial p}{\partial z} + \mu \left[ \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right] = \rho \left[ v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right]$$

Again, the open channel flow is predominantly only in y-direction. The variations of velocities in vertical direction may be neglected.

i.e.,  $v = v_{avg}(z)$  (i.e., the velocity in the y-direction is averaged over vertical direction at any cross section).

i.e., The dependents you can see are: v, w, p

 $\rightarrow$  The boundary conditions are:

$$v(y = 0, z) = v_1$$
  

$$v(y = L, z) = v_2$$
  

$$w(y, z = 0) = 0$$
  

$$p(y = 0, z) = \rho g(h_1 - z)$$
  

$$p(y = L, z) = \rho g(h_2 - z)$$
  

$$w[0 < y < L_1, z = h_1] = 0$$
  

$$w[L_1 < y < L, z = h_2] = 0$$