04/04/2017

<u>LECTURE – 33</u>

Geometric Interpretation of Stream Function:

In the last class, you came to know about the different types of boundary conditions that needs to be applied to solve the governing equations for fluid flow:

i.e. the conservation of mass, the conservation of linear momentum, the conservation of energy.

You were told that, the most general way of solving a fluid flow problem is to simultaneously solve the above equations on conservation principles & get the values of the <u>unknown</u> or <u>dependent variables</u> (i.e. ρ , p, u, v, w, T).

However, we as human beings, it may be difficult for us to solve all three simultaneously even for a simple fluid flow.

Moreover, considering engineering applications, there may no need to solve all of them simultaneously.

You can reduce the dependent variables & the equations as per the situation.

In that light, we introduced you the concept of stream function for <u>horizontal two dimensional</u> flow.

i.e. you know that flow varies only in x & y directions & assuming <u>isothermal conditions</u> as well as incompressible flow, the continuity equation is:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

(As, $\frac{\partial w}{\partial z} = 0$; no variations in vertical direction)

For solving benefit, you were introduced a function $\psi = \psi(x, y)$ such that

$$\frac{\partial}{\partial x}\left(\frac{\partial \psi}{\partial y}\right) + \frac{\partial}{\partial y}\left(-\frac{\partial \psi}{\partial x}\right) = 0$$

i.e, this means that

$$u = \frac{\partial \psi}{\partial y} \& v = -\frac{\partial \psi}{\partial x}$$

So, the governing equation for motion becomes unknown in only one quantity ψ . How??

Rather than giving in most general form: Recall the velocity gradient term.

It consisted of strain rate tensor & vorticity tensor.

That is, a fluid flow consist of rate of deformation & rate of rotation.

i.e, vorticity tensor =
$$\frac{1}{2} \left[\frac{\partial v_i}{\partial x_j} - \frac{\partial v_j}{\partial x_i} \right]$$

Associated with vorticity tensor, we can define a vector called vorticity vector $\vec{q} = \nabla \times \vec{v}$

Or,
$$\overrightarrow{q_i} = \varepsilon_{ijk} \frac{\partial v_k}{\partial x_j}$$

That is, the vorticity vector is actually the curl of the velocity vector.

So, in the given two dimensional flow, if the flow is irrotational, that means

$$\vec{\nabla} \times \vec{v} = 0$$

i.e, det
$$\begin{pmatrix} \hat{i} & j & k \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ \frac{\partial\psi}{\partial y} & -\frac{\partial\psi}{\partial x} & 0 \end{pmatrix} = 0$$
 or, $\frac{\partial\psi^2}{\partial x^2} + \frac{\partial\psi^2}{\partial y^2} = 0$

That is, for <u>irrotational flows of inviscid fluids</u> we can have the governing equation in steadystate conditions as:

$$\frac{\partial \psi^2}{\partial x^2} + \frac{\partial \psi^2}{\partial y^2} = 0$$

You need to now solve only for ψ in the given x, y domain.

(Please note that this is possible only for irrotational, inviscid flows.)

Geometric Interpretation of ψ :

Recall, we had earlier defined streamlines.

A streamline is a line, which is tangent to velocity vector \vec{v} everywhere at a given instant.



The position vector is \vec{dr} for a particle or at a mathematical point.

 $\overrightarrow{dr} = dx\hat{i} + dy\,j + dzk$

Now the velocity vector is tangent to position vector or parallel.

The components of velocity vector & position vector should match.

$$\vec{dr} = dx\hat{i} + dy \, j + dzk$$
$$\vec{v} = u\hat{i} + v \, j$$

i.e, $\frac{dx}{u} = \frac{dy}{v} = \frac{|dr|}{|\vec{v}|}$ (for both of them to be parallel)

As per streamline definition, $u = \frac{\partial \psi}{\partial y} \& v = -\frac{\partial \psi}{\partial x}$

As,
$$\frac{dx}{u} = \frac{dy}{v}$$

i.e., vdx - udy = 0 (equation for a streamline)

i.e.,
$$-\frac{\partial \psi}{\partial x}dx - \frac{\partial \psi}{\partial y}dx = 0$$

i.e.,
$$\frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dx = 0 = d\psi$$
 (Calculus Principle)

this means that $d\psi = 0$

Or, along a streamline, $\psi = \text{constant}$

So, for a given flow problem, if we solve for ψ , then subsequently you can plot streamlines or lines of constant ψ 's.



For a <u>control surface</u> (Not stream line)

The net outflow through the control surface between two point (1) & (2) :

$$dQ = (v.n)dA$$

Taking unit width into the paper:

dA = ds *1 = ds

$$dQ = (u\hat{i} + vj)(\frac{dy}{ds}\hat{i} - \frac{dx}{ds}j)(ds \times 1)$$
$$= (\frac{\partial\psi}{dy}\hat{i} - \frac{\partial\psi}{dx}j)(\frac{dy}{ds}\hat{i} - \frac{dx}{ds}j)(ds \times 1)$$
i.e, $dQ = (\frac{\partial\psi}{dx}dx + \frac{\partial\psi}{dy}dy) = d\psi$
$$dQ = (\frac{\partial\psi}{dx}dx + \frac{\partial\psi}{dy}dy) = d\psi$$

That is change in ψ across the element surface is equal to the volume flow through the element. Volume flow between any two stream lines $\psi_1 \& \psi_2 = \psi_2 - \psi_1 = \int_1^2 d\psi = \int_1^2 dQ$