

CONTINUITY OF THREE PHASES IN

A THREE-Dimensionally CONSOLIDATING POROUS MEDIA

In the last class, we started discussing about the mass conservation equations for three phases
→ solids, liquids, and gases
in a consolidating porous media

Recall in the control volume of porous media:



- Density of solids = ρ_s
- Density of liquid = ρ_l
- Density of gas = ρ_g

It is assumed that mass of solids in the control volume will not change, although the solids move at velocity \vec{v}_s .

- Mass flux for solid phase, $\vec{J}_s = \rho_s \vec{v}_s$
- " " for liquid phase, $\vec{J}_l = \rho_l \vec{v}_l$
- " " for gaseous phase, $\vec{J}_g = \rho_g \vec{v}_g$

Recall the mass conservation for liquid in saturated porous media:

$$\nabla \cdot (\rho_l \vec{q}) + \frac{\partial (\rho_l s)}{\partial t} = 0$$

Similarly we can have mass conservation equation for each phase as below:

(2)

$$\begin{array}{l}
 \text{Liquids: } \nabla \cdot \vec{J}_l + \frac{\partial}{\partial t} (n_s \rho_l) = 0 \\
 \text{Gas: } \nabla \cdot \vec{J}_g + \frac{\partial}{\partial t} ((1-n_s) \rho_g) = 0 \\
 \text{Solids: } \nabla \cdot \vec{J}_s + \frac{\partial}{\partial t} ((1-n) \rho_s) = 0
 \end{array} \quad \left. \vphantom{\begin{array}{l} \text{Liquids:} \\ \text{Gas:} \\ \text{Solids:} \end{array}} \right\} \rightarrow \textcircled{1}$$

Recall in the earlier section, we described the relative specific discharge of liquid in the saturated porous media, where the solids were moving at a velocity \vec{V}_s .

Similarly we need to describe the specific discharge of liquid w.r.t. the moving solids here also

$$\text{i.e. } \vec{q}_{rel} = -K \nabla \phi^*$$

(Note that the porous media is isotropic & homogeneous)

$$\text{i.e. } \vec{q}_{rel} = (\vec{V}_l - \vec{V}_s) n_s$$

where $\vec{V}_l \rightarrow$ actual velocity of liquid w.r.t. fixed coordinates
 $\vec{V}_s \rightarrow$ velocity of solids in the control volume.

$\phi^* \rightarrow$ piezometric head for compressible fluid.

$\rho_l \rightarrow \rho_l(p)$ (i.e. function of liquid pressure)

\Rightarrow The equations of state for the three phases ~~are~~ that may be followed are:

$$\begin{array}{l}
 \rho_s = \text{constant} \\
 \rho_l = \rho_{ol} \exp(\beta p) \\
 \rho_g = \rho_{og} \left(\frac{p}{p_{og}} \right)
 \end{array} \quad \left. \vphantom{\begin{array}{l} \rho_s \\ \rho_l \\ \rho_g \end{array}} \right\} \rightarrow \textcircled{2}$$

(3)

As discussed earlier, ρ_{ol} , ρ_{og} , etc. are reference densities.

Utilizing these relations in mass conservation equations (1):

For solids:

$$\nabla \cdot \vec{J}_s + \frac{\partial}{\partial t} ((1-n)\rho_s) = 0$$

$$\text{i.e. } \nabla \cdot (\rho_s \vec{q}_s) + \frac{\partial}{\partial t} ((1-n)\rho_s) = 0$$

$$\text{As } \rho_s \approx \text{a constant} \quad \nabla \rho_s = 0 \quad \text{and} \quad \frac{\partial \rho_s}{\partial t} = 0$$

\therefore We have:

$$\nabla \cdot \vec{q}_s + \frac{\partial}{\partial t} (1-n) = 0$$

$$\text{or } \frac{\partial n}{\partial t} = (1-n) \nabla \cdot \vec{V}_s + \vec{V}_s \cdot \nabla (1-n)$$

$$\therefore \vec{q}_s = (1-n) \vec{V}_s$$

$$\therefore \frac{\partial n}{\partial t} = \nabla \cdot [(1-n) \vec{V}_s] \quad \rightarrow (3)$$

For liquids:

$$\nabla \cdot \vec{J}_l + \frac{\partial}{\partial t} (n \rho_l \rho_l) = 0$$

$$\text{or } \vec{J}_l = \rho_l \vec{q}_l = \rho_l n \rho_l \vec{V}_l$$

$$\therefore \nabla \cdot [\rho_l n \rho_l \vec{V}_l] + \frac{\partial}{\partial t} (n \rho_l \rho_l) = 0 \quad \rightarrow (4)$$

(4)

In gas:

$$\nabla \cdot \vec{J}_g + \frac{\partial}{\partial t} ((1 - s_l) n p_g) = 0$$

ie. $\nabla \cdot [(1 - s_l) n p_g \vec{V}_g] + \frac{\partial}{\partial t} (n p_g (1 - s_l)) = 0 \rightarrow (5)$

Equations (3), (4), and (5) are to be solved simultaneously for such multi-phase systems.

CONTINUITY EQUATION FOR FLOW IN CONFINED AND

LEAKY AQUIFERS

In groundwater hydrology you will often come up with terms like - aquifers.

You have confined, unconfined, and leaky aquifers in nature.

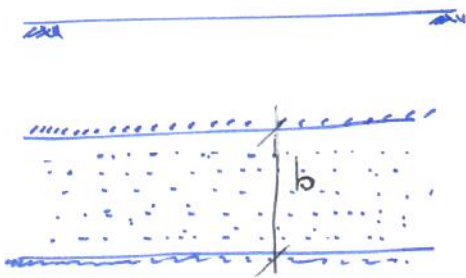
\Rightarrow The theory of mass conservation developed in general for any porous media are very much applicable for mass conservation in aquifers.

\rightarrow Let us revisit the mass conservation equation for aquifers in this portion.

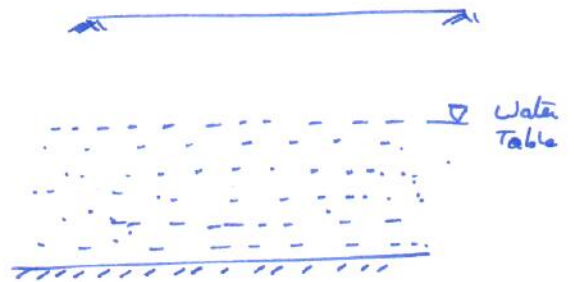
\Rightarrow An aquifer is a water bearing strata in subsurface of earth.

(5)

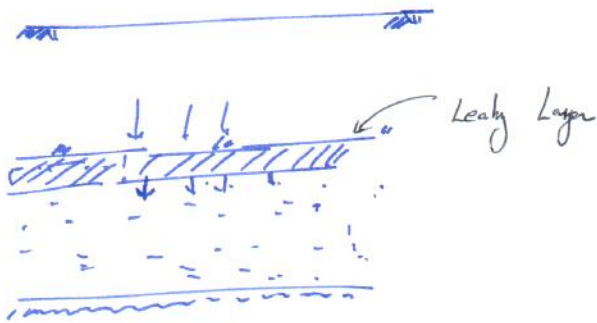
A confined aquifer



An unconfined aquifer



A leaky aquifer



→ Compared to flow in general in porous media, aquifer flows are typically horizontal in nature.

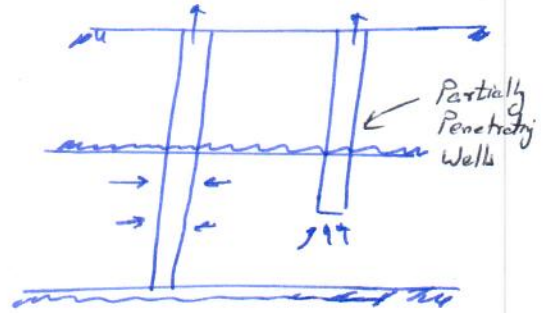
→ We may also approximate flow in aquifers as horizontal.

→ The significance of horizontal flow approximations in aquifers are that

- * In confined aquifers the flow is always in $x-y$ plane (No vertical flow)
- * In leaky aquifers, although there are some quantities that fill the aquifer from top layers, still the basic flow is horizontal. The vertical flow will be considered only as a source or sink to the control volume.

(6)

→ However this approximation may not be fully true for partially penetrating wells



⇒ For aquifer flows:

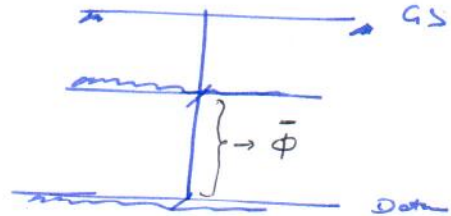
The piezometric head $\phi = \phi(x, y, z, t)$ in actual

three-dimensional flows:

However two-dimensional flows may be considered:

$$\bar{\phi} = \bar{\phi}(x, y, t)$$

where $\bar{\phi}$ is the average of piezometric head taken along a vertical line.



⇒ In groundwater aquifers, we consider the water as incompressible. ∴ Variations in S_e over space and time are neglected.

⇒ For a homogeneous isotropic aquifer, we have

$$\text{Transmissivity, } T = Kb$$

where $K \rightarrow$ hydraulic conductivity
 $b \rightarrow$ confined aquifer thickness

(7)

In Confined Aquifers

⇒ Transmissivity, $T = \bar{K} b$

\bar{K} → average hydraulic conductivity over a vertical line.

(∵ $K = K(x, y)$)

$$\bar{K} = \frac{1}{b} \int_0^b K(z) dz$$

⇒ Aquifer Storage:

Volume of water (ΔU_w) released from aquifer storage per unit horizontal area of aquifer and per unit decline of the average piezometric head in the aquifer

$$S = \frac{\Delta U_w}{\Delta A \Delta \phi}$$



⇒ Specific Storage:

Volume of water released from aquifer storage per unit bulk volume of aquifer per unit decline of piezometric head (S_s).

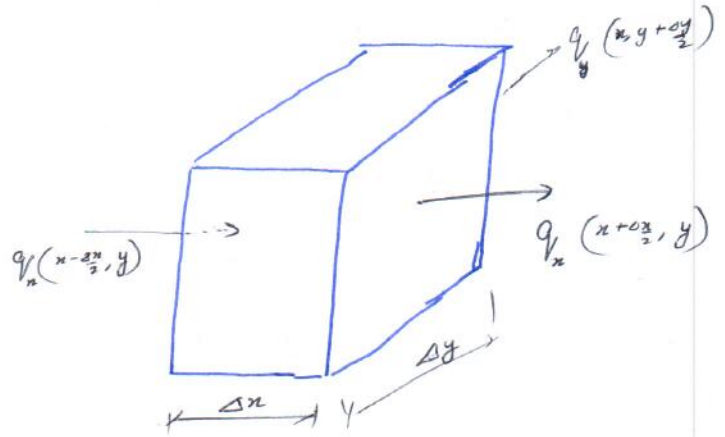
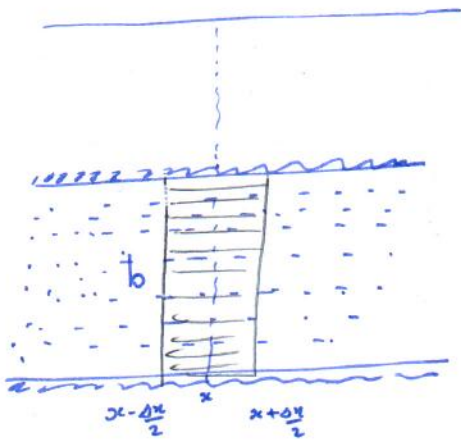
$$S = S_s b$$



⇒ To develop the continuity equation:

Let us consider the confined aquifer of thickness b and let us use the control volume approach:

(8)



The Control Volume

Mass Inflow in the x-direction = $\rho q_x(x - \frac{\Delta x}{2}, y) \cdot b \cdot \Delta y$

Mass Outflow in the x-direction = $\rho q_x(x + \frac{\Delta x}{2}, y) \cdot b \cdot \Delta y$

∴ Net mass outflow in the x-direction = $\rho [q_x(x + \frac{\Delta x}{2}, y) - q_x(x - \frac{\Delta x}{2}, y)] \Delta y b$

∴ Net mass outflow in the y-direction = $\rho [q_y(x, y + \frac{\Delta y}{2}) - q_y(x, y - \frac{\Delta y}{2})] \Delta x b$

Reynolds Transport Theorem for mass conservation

$$\frac{DB}{Dt} = 0 = \frac{\partial}{\partial t} \iiint \rho \, dV + \iint_{CS} \rho \mathbf{V} \cdot \hat{\mathbf{n}} \, dA$$

Here $B = \text{mass of water}$ and $\frac{DB}{Dt} = 0$, $\rho = 1.0$

$$\therefore 0 = \frac{\partial}{\partial t} \iiint \rho \, dV + \iint_{CS} \rho (\mathbf{q} \cdot \hat{\mathbf{n}}) \, dA \quad \text{for porous CV.}$$

As liquid is incompressible ρ is cancelled.

$$0 = \frac{\partial}{\partial t} \iiint dV + \iint_{CS} (\mathbf{q} \cdot \hat{\mathbf{n}}) \, dA \quad \rightarrow \textcircled{6}$$