

CONSERVATION EQUATIONS IN POROUS MEDIA

Recalling the conservation equations described in the last classes (for porous media)

* The local volume conservation equation for an incompressible fluid is:

$$\left\langle \frac{\partial V'_s}{\partial t} \right\rangle = 0 \quad \rightarrow \textcircled{1}$$

* The REV based volume conservation equation for an incompressible fluid in porous media:

$$\frac{\partial}{\partial x_j} (n \bar{V}'_j) = 0 \quad \rightarrow \textcircled{2}$$

$$\frac{\partial q_j}{\partial x_j} = 0$$

* Mass conservation equation for a species α in the solution (or fluid) in a porous medium

Assuming $I_\alpha = 0$

The local conservation equation is:

$$\left\langle \frac{\partial \rho_\alpha}{\partial t} \right\rangle = \left\langle \frac{\partial}{\partial x_i} \left(D_{\alpha\beta} T_{ij}^* \frac{\partial \rho_\alpha}{\partial x_j} \right) \right\rangle - \left\langle \frac{\partial}{\partial x_i} (\rho_\alpha V'_i) \right\rangle$$

* The mass conservation equation for species α in fluid in porous medium averaged over entire void space in REV:

$$\frac{\partial \bar{\rho}_\alpha}{\partial t} = \frac{\partial}{\partial x_i} \left(D_{\alpha\beta} \overline{T_{ij}^*} \frac{\partial \bar{\rho}_\alpha}{\partial x_j} \right) - \frac{\partial}{\partial x_i} \overline{\rho_\alpha V'_i} - \overline{\frac{\rho_\alpha V'_i}{n}} \frac{\partial n}{\partial x_i} \quad \rightarrow \textcircled{4}$$

(2)

This REV averaged mass conservation equation for specie α can also be written in following form:

For incompressible liquid (assuming $n = \text{constant}$)

$$\frac{\partial \bar{S}_\alpha}{\partial t} = \frac{\partial}{\partial x_i} \left[(\underline{D}_{ij} + D_{\alpha\beta} \overline{T}_{ij}^*) \frac{\partial \bar{S}_\alpha}{\partial x_j} \right] - \bar{V}_i' \frac{\partial \bar{S}_\alpha}{\partial x_i}$$

Suggesting a second rank tensor say A_{ij} as \underline{A} symbolically, \rightarrow (5A)

$$\frac{\partial \bar{S}_\alpha}{\partial t} = \nabla \cdot [(\underline{D} + D_{\alpha\beta} \overline{T}^*) \nabla \bar{S}_\alpha] - \bar{\mathbf{V}}' \cdot \nabla \bar{S}_\alpha \rightarrow (5B)$$

where $\underline{D} \rightarrow$ coefficient of mechanical dispersion tensor

$D_{\alpha\beta} \overline{T}^* \rightarrow$ coefficient of molecular diffusion tensor

If $n \neq \text{constant}$, then

$$\begin{aligned} \frac{\partial \bar{S}_\alpha}{\partial t} = & \frac{\partial}{\partial x_i} \left[(\underline{D}_{ij} + D_{\alpha\beta} \overline{T}_{ij}^*) \frac{\partial \bar{S}_\alpha}{\partial x_j} \right] - \bar{V}_i' \frac{\partial \bar{S}_\alpha}{\partial x_i} \\ & - \frac{\bar{S}_\alpha}{n} \bar{V}_i' \frac{\partial n}{\partial x_i} \end{aligned}$$

* We can also have mass conservation for entire fluid

\rightarrow Averaged over cross sectional area:

$$\left\langle \frac{\partial S}{\partial t} \right\rangle = \left\langle \frac{\partial}{\partial x_i} \left[D_{\alpha\beta} \overline{T}_{ij}^* \frac{\partial S}{\partial x_j} \right] - \frac{\partial}{\partial x_i} (S \bar{V}_i') \right\rangle$$

\rightarrow (6)

(3)

* The mass conservation of the entire multi-species fluid averaged over the void spaces of the REV is given as:

(Assuming $n = \text{constant}$)

$$\frac{\partial \bar{S}}{\partial t} = \frac{\partial}{\partial x_i} \left[(D_{ij} + D_{sp} \overline{T_{ij}^*}) \frac{\partial \bar{S}}{\partial x_j} \right] - \frac{\partial}{\partial x_i} (\bar{S} \bar{v}_i')$$

→ (7)

* Similarly we can apply conservation of linear momentum also to the fluid in the void space in REV.

→ We can do local averaging

$$\left\langle \bar{v}_i^* + \frac{\beta \rho}{\mu} \frac{\partial \bar{v}_i^*}{\partial t} \right\rangle = - \left\langle \frac{\beta T_{ij}^*}{\mu} \left(\frac{\partial p}{\partial x_j} + \rho g \frac{\partial z}{\partial x_j} \right) \right\rangle$$

→ (8)

where

\bar{v}_i^* → Volume Mass averaged velocity vector
 ρ → density of entire multi-species fluid
 μ → dynamic viscosity
 β → conductance of a channel. It's dimension L^2 .
 (also function of the shape of channel's cross section).

* The REV averaged conservation of linear momentum is:

$$\overline{\bar{v}_i^*} + \overline{\beta \left(\frac{\rho}{\mu} \right) \frac{\partial \bar{v}_i^*}{\partial t}} = - \overline{\beta T_{ij}^*} \left[\frac{1}{\mu} \frac{\partial \bar{p}}{\partial x_j} + \frac{\bar{\rho}}{\mu} g \frac{\partial z}{\partial x_j} \right]$$

→ (9)

You may see that $n \overline{\beta T_{ij}^*} = k_{ij}$ permeability of the medium.

(4)

For liquids with its density fluctuation $\bar{\rho}^{\circ}$ such as $|\frac{\bar{\rho}^{\circ}}{\bar{\rho}}| \ll 1$

Dynamic viscosity, $|\frac{\bar{\mu}^{\circ}}{\bar{\mu}}| \ll 1$,

In such situations we can assume the momentum equation as:

$$\bar{V}_i^* + \frac{\bar{\beta} \bar{\rho}}{\bar{\mu}} \frac{\partial \bar{V}_i^*}{\partial t} = - \frac{k_{ij}}{n \bar{\mu}} \left(\frac{\partial \bar{p}}{\partial x_j} + \bar{\rho} g \frac{\partial z}{\partial x_j} \right)$$

→ (10)

If the mass averaged velocity is replaced by volumetric averaged velocity \bar{V}_i' , then

$$\bar{V}_i' - D_{\alpha\beta} \bar{T}_{ij}^* \frac{1}{\bar{\rho}} \frac{\partial \bar{\rho}}{\partial x_j} + \frac{\bar{\beta} \bar{\rho}}{\bar{\mu}} \frac{\partial}{\partial t} \left[\bar{V}_i' - D_{\alpha\beta} \bar{T}_{ij}^* \frac{1}{\bar{\rho}} \frac{\partial \bar{\rho}}{\partial x_j} \right] = - \frac{k_{ij}}{n \bar{\mu}} \left(\frac{\partial \bar{p}}{\partial x_j} + \bar{\rho} g \frac{\partial z}{\partial x_j} \right)$$

→ (11)

If the flux due to molecular diffusion based on density gradient is such that:

$$\left| D_{\alpha\beta} \bar{T}_{ij}^* \frac{\partial \bar{\rho}}{\partial x_j} \right| \ll \left| \bar{\rho} \bar{V}_i^* \right| \quad \text{then}$$

$$\bar{V}_i' + \left(\frac{\bar{\beta} \bar{\rho}}{\bar{\mu}} \right) \frac{\partial \bar{V}_i'}{\partial t} = - \frac{k_{ij}}{\bar{\mu}} \left(\frac{\partial \bar{p}}{\partial x_j} + \bar{\rho} g \frac{\partial z}{\partial x_j} \right)$$

→ (12)

(5)

where

$q_i \rightarrow$ Specific discharge vector

For laminar flows in porous media (also slow creeping motion), the local acceleration $\frac{\bar{\rho} \bar{s}}{\bar{\mu}} \frac{\partial q_i}{\partial t} \approx 0$

\therefore We will get:

$$q_i = - \frac{k_{ij}}{\bar{\mu}} \left(\frac{\partial \bar{p}}{\partial x_j} + \bar{s} g \frac{\partial z}{\partial x_j} \right) \rightarrow (13)$$

Note:

$k_{ij} \rightarrow$ Permeability tensor

$\bar{p} \rightarrow$ average of pressure in fluid over REV

$\bar{s} \rightarrow$ average of density of entire fluid in REV

For homogeneous incompressible fluid, you will have

$$\bar{s} = s = \text{a constant}$$

$$\bar{\mu} = \mu = \text{a constant}$$

$$\therefore q_i = - \frac{k_{ij} s g}{\mu} \frac{\partial}{\partial x_j} \left(\frac{\bar{p}}{s g} + z \right)$$

or

$$\vec{q} = - \frac{k s g}{\mu} \nabla \cdot \left(\frac{\bar{p}}{s g} + z \right)$$

} \rightarrow (14)

(6)

Equation (14) is the commonly used equation for specific discharge of a homogeneous, incompressible liquid in a porous medium.

You may also see that the term

$$\frac{K_{ij} \rho g}{\mu} = K_{ij}$$

↓
The hydraulic conductivity tensor.

$$\text{Also } \frac{\bar{P}}{\rho g} + z = \bar{\Phi} \Rightarrow \text{The piezometric head}$$

$$\therefore \boxed{q_i = -K_{ij} \frac{\partial \bar{\Phi}}{\partial x_j}}$$

Pr 2-2

Derive the continuity eqn