

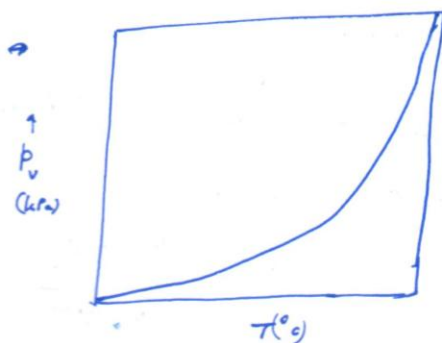
SECONDARY PROPERTIES OF FLUID

- * In the last class, we described about viscosity.
- * Subsequently we mentioned about Newtonian and Non-Newtonian fluids.
- * We worked out an example problem on shear stress.
- * In the class notes, we described about another fluid property - vapor pressure.
- * Due to time constraint, that portion was not lectured. However, I hope that you might have gone through those portions in the lecture notes.

Revisiting them:

Vapor Pressure

→ It is the pressure at which a liquid boils and is in equilibrium with its own vapor.



→ The curve here shows the equilibrium vapor pressure at which liquid boils.

→ This vapor pressure ^{curve} is also called saturated vapor pressure curve.

(2)

- If the liquid pressure is greater than the saturated vapor pressure, the only exchange between liquid and vapor is evaporation at interface
- If the liquid pressure (or ambient pressure) falls below the vapor pressure, vapor bubbles begin to appear in the liquid.
- When the liquid pressure drops below the saturated vapor pressure due to flow phenomenon, the process is called CAVITATION.

Note: → If water is accelerated from rest to approximately 15 m/s, the pressure of it drops by nearly 1 atm.
You know, $1 \text{ atm} = 1.01325 \times 10^5 \text{ N/m}^2$
 $= 101.325 \text{ kPa}$

→ When water is heated to 100°C , its vapor pressure will be 101.325 kPa .

→ As told earlier, there can be flow induced reduction in ~~vapor~~ ambient pressure.

Cavitation Number,
$$Ca = \frac{p_a - p_v}{\frac{1}{2} \rho V^2}$$

- p_a → ambient liquid pressure
- p_v → vapor pressure
- V → characteristic flow velocity
- ρ → density of fluid.

(3)

Example: (As adopted from FM White's "Fluid Mechanics")

A torpedo moving in fresh water at 15°C . The minimum pressure point is $p_{\min} = p_0 - 0.35 \rho V^2$, where p_0 is given as 120 kPa , ρ is water density, V is torpedo velocity. Estimate the velocity at which cavitation bubbles will form on torpedo. The density vs temperature as well as vapor pressure vs temperature data are as given.

$T^\circ\text{C}$	$\rho \text{ (kg/m}^3\text{)}$
0	1000
10	1000
20	998
30	996

$T^\circ\text{C}$	$p_v \text{ (kPa)}$
0	0.611
10	1.227
20	2.337
30	4.242
40	7.375
...	...

Solution

Cavitation bubbles start to form when liquid pressure equals the vapor pressure at that temperature.

→ So let $p_{\min} = p_v$ for this problem.

$$p_{\min} = p_0 - 0.35 \rho V^2 = 120 \times 10^3 - 0.35 \times 999 \times V^2$$

$$p_v \text{ at } 15^\circ\text{C} \approx 1.80 \text{ kPa} = 1800 \text{ Pa}$$

$$\therefore 1800 = 120 \times 10^3 - 0.35 \times 999 \times V^2$$

$$\therefore V^2 = 338, \quad \text{or } \underline{\underline{V = 18.4 \text{ m/s}}}$$

Surface Tension

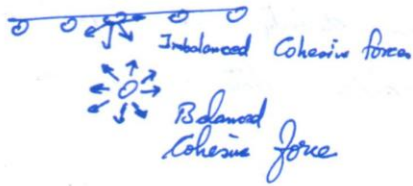
It is the maximum energy level a fluid can store without breaking apart.

(4)

→ It describes the interface between two fluids

* say air-water interface
oil-water interface, etc.

→ Interfacial tension acts between two fluids

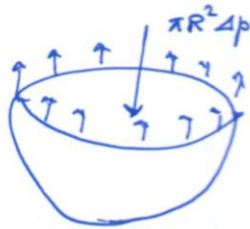


→ You can see imbalanced cohesive forces for the fluid molecules at the interface.

→ These imbalanced forces create tension in the interface. It can be given as σ (N/m).

→ At static equilibrium, the interface forces and other forces should balance.

e.g. If the interface is curved, the mechanical balance shows that there is a pressure difference across the interface.



$$\pi R^2 \Delta p = 2\pi R \sigma$$

$$\therefore \Delta p = \frac{2\sigma}{R}$$

e.g. In a ~~spherical~~ droplet



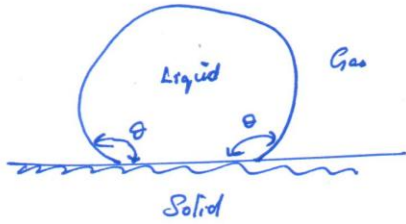
$$\Delta p_{\text{droplet}} = \frac{2\sigma}{R}$$



Balancing forces,
$$\Delta p = \sigma \left(\frac{1}{R_1} + \frac{1}{R_2} \right)$$

→ The droplet on a solid surface will be having contact angle, θ .

(5)



→ The contact angle θ suggests something about liquid-gas-solid interface.

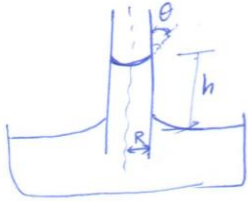
If $\theta < 90^\circ$; liquid wets the solid
 If $\theta > 90^\circ$; liquid is non-wetting

→ While doing equilibrium (or static) force balance, the contact angle also needs to be taken.

→ The capillary rise in tubes also depends on surface tension. See the following example.

Example (Adapted from FM WHITE: Fluid Mechanics)

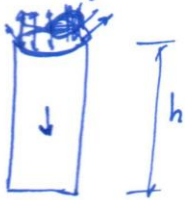
Derive the expression for change in height h in a circular tube of liquid with surface tension, σ and contact angle θ .



Solution.

In static equilibrium, the forces should balance in each direction.

Let us balance forces in vertical direction at the interface in the free body diagram



$$\begin{aligned} \text{Force due to weight} &= \rho g \pi R^2 h \\ \text{Surface tension force} &= 2\pi R \sigma \cos\theta \end{aligned}$$

$$\sum F_y = 0; \quad 2\pi R \sigma \cos\theta - \rho g \pi R^2 h = 0$$

$$\text{or } h = \frac{2\sigma \cos\theta}{\rho g R}$$

→ The capillary height increases inversely with the capillary tube radius R .

⑥

⇒ In due course, you will see what is

- * Streamline
- * Pathline
- * Streakline

⇒ We will be using

- * Control-volume or integral analysis
- * Infinitesimal system or differential analysis
- * Experimental study or the dimensional analysis

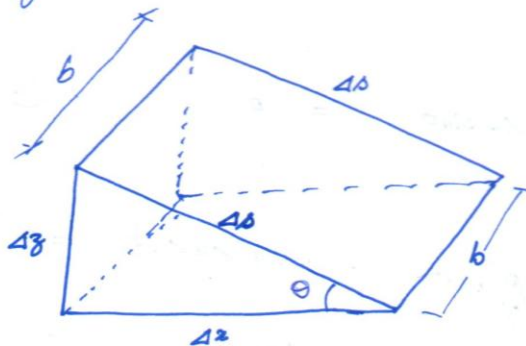
for studying fluid mechanics

⇒ Recall the fundamental laws like:

- * Conservation of mass
- * Conservation of linear momentum
- * Conservation of energy, etc.

PRESSURE DISTRIBUTION IN A FLUID

- When the fluid velocity is zero, we call it as hydrostatic conditions.
- The pressure of the liquid varies with respect to the weight of fluid.
- As discussed earlier, a fluid at rest cannot support shear stress.
- Let us describe the equilibrium of forces (static liquid) of a small wedge of fluid at rest.



- Recall your engineering mechanics of study about free body diagrams. As this is static liquid all the forces need to be balanced.
- Obvious, from the figure, the forces in y -direction balance. Still we can work it out.
- $$\sum F_x = 0 ; \quad \sum F_y = 0 ; \quad \sum F_z = 0 .$$

②

As it is a static liquid, let us suggest that forces act into the plane in respective directions.

→ let p_x be force per unit area acting on the plane $b \Delta z$.

→ let p_z be the force per unit area acting on the plane $b \Delta x$

→ p_y be the force per unit area acting on the planes $\Delta x \Delta z$ in front side and $\Delta x \Delta z$ in back side.

→ p_o be the force per unit area on the plane $b \Delta s$.

∴ In $\sum F_y = 0$

$$p_y \Delta x \Delta z - p_y \Delta x \Delta z = 0 \rightarrow \textcircled{1}$$

(Both forces are same)

In $\sum F_x = 0$;

$$p_x b \Delta z - p_o b \Delta s \sin \theta = 0 \rightarrow \textcircled{2}$$

In $\sum F_z = 0$;

$$-p_o b \Delta s \cos \theta + p_z b \Delta x - \frac{1}{2} \rho g \Delta x \Delta z b = 0 \rightarrow \textcircled{3}$$

From geometry -

$$\begin{aligned} \Delta s \cos \theta &= \Delta x \\ \Delta s \sin \theta &= \Delta z \end{aligned}$$

∴ In $\textcircled{2}$; $p_x b \Delta z - p_o b \Delta z = 0$; or $p_x = p_o$

In $\textcircled{3}$; $-p_o b \Delta x + p_z b \Delta x - \frac{1}{2} \rho g b \Delta x \Delta z = 0$

$$\text{or } p_z = p_o + \frac{1}{2} \rho g \Delta z$$

In $\lim_{\substack{\Delta z \rightarrow 0 \\ \Delta x \rightarrow 0}}$; $p_z = p_o = p_x = p_y = p = \text{pressure}$

That is at a static point, pressure is a static scalar property without any orientation.