

TURBULENT FLOWS

Yesterday, we discussed about laminar flow in pipes.

→ We discussed about head loss and for circular (or round pipes), if the flow is laminar, then

$$h_f = \frac{32 \mu L V}{\rho g D^2} = \frac{128 \mu L Q}{\pi \rho g D^4} \rightarrow (1)$$

As the general form of head loss is :

$$h_f = f \frac{L}{D} \frac{V^2}{2g}, \rightarrow (2)$$

we can deduce the Poiseuille laminar flow friction factor,  $f_{\text{laminar}}$  by comparing (1) and (2).  
You see that the friction factor,  $f = \frac{64}{Re}$ .

⇒ In turbulent flows, the fluctuation of velocities within a cross section itself is huge.  
That is, you may find it difficult to use the differentiated equations for flow for turbulent condition.

(2)

For turbulent pipe flow, you need ~~to~~ not solve the differential equations at present.

Many scientists have worked on pipe flow and have deduced relations to find the friction factor.

e.g: In 1935, Prandtl found the following empirical relation between friction factor and Reynolds number in turbulent pipe flow

$$\frac{1}{\sqrt{f}} = 2.0 \log \left[ \frac{Re \sqrt{f}}{25} \right] - 0.8$$

From this, you can deduce  $\Delta h$  head loss,

$$h_f = f \frac{L}{D} \frac{V^2}{2g}$$

Note:  $\rightarrow$  If the pipe is horizontal, you may then see that

$$h_f = \frac{\Delta p}{\rho g}$$

$$\text{or } \Delta p = \rho g h_f$$

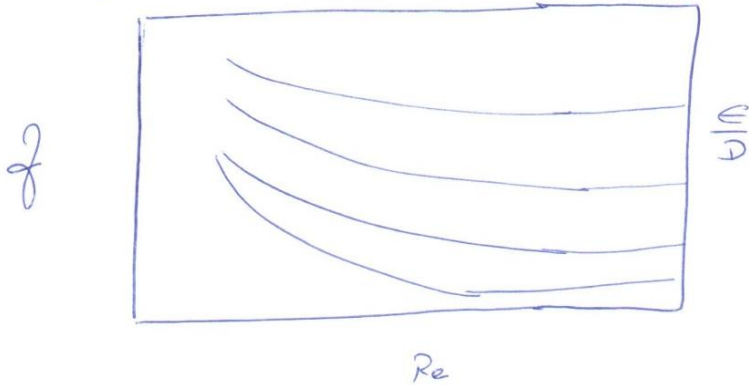
where  $h_f$  is already evaluated using friction factor.

$\Rightarrow$  The Moody's chart for pipe friction is a well-established chart for friction factor  $f$  versus Reynolds number. It uses the formula:

$$\frac{1}{\sqrt{f}} = -2.0 \log \left[ \frac{\epsilon/D}{3.7} + \frac{2.51}{Re \sqrt{f}} \right]$$

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This Moody's chart is used in most of the standard-design of pipe flow problems.



Recall  
 $D \rightarrow$  diameter of pipe

Here the  $\epsilon$  is the roughness thickness.

Some of the recommended roughness values are:

Material	Condition	$\epsilon$	
		mm	mm
Steel	Sheet Metal, New	0.05	
	Stainless, New	0.002	
	Commercial, New	0.046	
	Riveted	3.0	
	Rusted	2.0	
Iron	Cast, New	0.26	
	Wrought, New	0.046	
	Galvanised, New	0.15	
	Asphalted, Cast	0.12	
Brass		0.002	
Plastic	Tube.	0.0015	
Glass	-	-	
Rubber	Smoothed	0.01	
Wood		0.5	
		2.0	
Concrete	Rough	2.0	
	Smooth	0.04	

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= The scientist Haaland has given an explicit relation to Moody's chart with less than 2% variation.

$$\frac{1}{\sqrt{f}} \approx -1.8 \log_{10} \left[ \frac{6.9}{Re} + \left( \frac{\epsilon/D}{3.7} \right)^{1.11} \right]$$

You may utilize this relation in turbulent flow computations.

Example: (As adapted from FM White's Fluid Mechanics)  
Oil with  $\rho = 900 \text{ kg/m}^3$  and kinematic viscosity,  $\nu = 0.00001 \text{ m}^2/\text{s}$  flows at  $0.2 \text{ m}^3/\text{s}$  through  $500 \text{ m}$  of  $200 \text{ mm}$ -diameter cast iron pipe. Determine a) the head loss, b) the pressure drop if the pipe slopes down at  $10^\circ$  in the flow direction.

Solution.

Given  $\rho = 900 \text{ kg/m}^3$ ,  $\nu = 0.00001 \text{ m}^2/\text{s}$

$$\therefore \mu = \rho \nu = 900 \times 0.00001 = 0.009 \frac{\text{kg}}{\text{m}\cdot\text{s}}$$

$$Q = 0.2 \text{ m}^3/\text{s}, \quad L = 500 \text{ m}, \quad D = 200 \text{ mm} = 0.2 \text{ m}$$

We are ~~considering~~ <sup>assuming</sup> steady and incompressible flow for this

case:

$$\therefore V = \frac{Q}{A} = \frac{0.2}{\frac{\pi}{4} \times (0.2)^2} = 6.4 \text{ m/s}$$

$$\text{Reynolds Number, } Re = \frac{\rho V D}{\mu} = \frac{900 \times 6.4 \times 0.2}{0.009}$$

$$= \underline{\underline{128000}} \gg 2300$$

Flow is turbulent.

$\Rightarrow$  We have to compute head loss:

(5)

→ The pipe material is cast iron

$$\therefore \epsilon = 0.26 \text{ mm}$$

$$\therefore \frac{\epsilon}{D} = \frac{0.26}{200} = 0.0013$$

From the explicit formula

$$\frac{1}{\sqrt{f}} = -1.8 \log_{10} \left[ \frac{6.9}{Re} + \left( \frac{\epsilon/D}{3.7} \right)^{1.11} \right]$$

$$\begin{aligned} \frac{1}{\sqrt{f}} &= -1.8 \log_{10} \left[ \frac{6.9}{128000} + \left( \frac{0.0013}{3.7} \right)^{1.11} \right] \\ &= -1.8 \times (-3.698) = 6.6566 \end{aligned}$$

$$\sqrt{f} = 0.1502 \quad ; \quad f = 0.0226$$

$$\begin{aligned} \therefore h_f &= f \frac{L}{D} \frac{V^2}{2g} = 0.0226 \times \frac{500}{0.2} \frac{(6.4)^2}{2 \times 9.81} \\ &\approx \underline{\underline{118 \text{ m}}} \end{aligned}$$

$$\therefore \underline{\underline{h_g = 118 \text{ m}}}$$

Pressure drop

$$\begin{aligned} h_g &= 43 + \frac{\Delta p}{\rho g} \\ \therefore \Delta p &= \left[ \frac{118}{\sin 10} + 118 \right] \times 900 \times 9.81 \\ \Delta p &= \left[ \frac{118}{\sin 10} + 118 \right] \times 900 \times 9.81 \\ \therefore 118 &= L \sin(10) + \frac{\Delta p}{\rho g} \\ \therefore \Delta p &= [118 - 500 \sin(10)] \times 900 \times 9.81 \\ &\approx 273699 \approx \underline{\underline{273700 \text{ Pa}}} \end{aligned}$$

(6)

⇒ You can now also think, what does a pump do?

→ If the hydraulic head is lower at a portion and you want to take water from that location, then a pump will provide additional head, so that overall head at that location increases and water will flow to the location of lower head.

⇒ The following types of design problems can be seen in Pipe flows.

- (i) Given  $D, L, V$  (or  $Q$ ),  $S, \mu, g$ , → compute head loss  $h_f$ .
- (ii) Given  $D, L, h_f, S, \mu, g$ , → compute velocity  $V$  or discharge  $Q$ .
- (iii) Given  $Q, L, h_f, S, \mu, g$  → compute diameter of the pipe
- (iv) Given  $Q, D, h_f, S, \mu, g$  → compute the pipe length  $L$